

# Thermolytic conversion of a bis(alkoxy)tris(siloxy)tantalum(V) single-source molecular precursor to catalytic tantala–silica materials

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## Abstract

The new complex  $(^i\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^t\text{Bu})_3]_3$  (**1**) was prepared via silanolysis of  $\text{Ta}(\text{O}^i\text{Pr})_5$  with  $(^t\text{BuO})_3\text{SiOH}$  and is a useful structural and spectroscopic (NMR, FTIR) model of Ta(V) on silica. The complex was also used to prepare tantalum-containing silica materials, via the thermolytic molecular precursor method (yielding  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ ) or by grafting **1** onto mesoporous SBA-15 silica (yielding a surface-supported tantala species, TaSBA-15). The solution phase thermolysis of **1** in nonpolar media afforded homogeneous, high-surface-area (ca.  $450 \text{ m}^2 \text{ g}^{-1}$ ) xerogels ( $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$ ) that are amorphous up to approximately  $1100^\circ\text{C}$ . A more silica-rich tantala–silica material ( $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ ) was prepared via a solution-phase co-thermolytic route with **1** and  $\text{HOSi}(\text{O}^t\text{Bu})_3$ , to yield a material with a Si/Ta ratio of 9/1. It was demonstrated that tantala–silica materials are active as catalysts for cyclohexene oxidation.  
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**Keywords:** Tantalum; Silicon; Molecular precursor route; Amorphous materials; Supported catalysts; Oxidation; Peroxides

## 1. Introduction

The rational design and development of new catalytic materials, for which the arrangements of atoms and nanostructures are well defined, remains a formidable challenge for chemists and materials scientists [1–3]. One method that has received considerable attention is the low-temperature sol–gel route, which can produce metal oxide materials through the hydrolysis and condensation of metal alkoxide precursors (typically in polar media) [4–6]. One drawback to this method is that the formation of homogeneous, mixed metal oxide materials is complicated by the inherently different hydrolysis rates for the various metal alkoxide precursors. Thus it is often difficult to optimize the homogeneity of the resultant materials, especially without special precautions and optimized experimental conditions [4–13].

One alternative to the sol–gel method relies on the use of single-source molecular precursors [14–22]. Such precursors possess a defined ratio of elements to be incorporated into the target material and provide a low-temperature, kinetically controlled pathway to homogeneous, mixed metal oxide materials. A number of such precursors, which are transition metal tris(*tert*-butoxy)siloxy complexes of the type  $\text{M}[\text{OSi}(\text{O}^t\text{Bu})_3]_n$ , have been prepared and studied [23–27]. These oxygen-rich molecular precursors can be thermolytically converted to amorphous, homogeneous transition metal oxide–silica materials. Upon heating (usually below  $200^\circ\text{C}$ ), these molecular precursors eliminate isobutylene and water to give the transition metal oxide–silica material, either in the solid state or in nonpolar media. Solution thermolyses of the molecular precursors afford high-surface-area xerogels upon air-drying.

Silica-supported group V materials are known to be potentially interesting alkene oxidation catalysts [28–35]. Although considerable attention has been devoted to vanadium and niobium silica-supported catalysts, only a few studies have addressed the synthesis of silica-supported tanta-

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lum alkene oxidation catalysts [29,30]. Here we report the synthesis and characterization of a single-source molecular precursor,  $(^i\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^t\text{Bu})_3]_3$  (**1**), and its thermolytic conversion to tantalum–silica materials. These materials have been studied as cyclohexene oxidation catalysts.

## 2. Experimental

### 2.1. General procedures

All manipulations were conducted under a nitrogen atmosphere with the use of standard Schlenk techniques, or in a Vacuum Atmospheres drybox, unless otherwise noted. Dry, oxygen-free solvents were used throughout. Benzene- $d_6$  was purified and dried by vacuum distillation from sodium/potassium alloy.

$\text{TaCl}_5$  was purchased from Strem Chemicals, Inc., and sublimed prior to use. *iso*-Propyl alcohol and triethylamine were purchased from Aldrich and distilled from calcium hydride prior to use. Cyclohexene was purchased from Aldrich and distilled prior to use. Aqueous hydrogen peroxide ( $\text{H}_2\text{O}_2$ ) (30%), cumene hydroperoxide (CHP) (80%), and *tert*-butyl hydroperoxide (TBHP) (5.5 M in decane) were purchased from Aldrich and used as received.  $\text{Ta}(\text{O}^i\text{Pr})_5$  [36],  $(^t\text{BuO})_3\text{SiOH}$  [37], and SBA-15 [38] were prepared as reported in the literature.

### 2.2. Synthesis of $(^i\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^t\text{Bu})_3]_3$ (**1**)

A pentane (20 ml) solution of  $(^t\text{BuO})_3\text{SiOH}$  (8.43 mmol) was added to a pentane (10 ml) solution of  $\text{Ta}(\text{O}^i\text{Pr})_5$  (1.67 mmol) in a Schlenk tube under flowing nitrogen at 0 °C. The reaction mixture was warmed to room temperature, and stirring was continued for 15 h. Subsequent removal of the volatile materials in vacuo (25 °C) yielded a white solid, at which point excess  $(^t\text{BuO})_3\text{SiOH}$  was sublimed away from the product (70 °C, 0.001 mm Hg, 4 h). The white solid was taken up in a pentane/toluene (ca. 1/1, vol/vol) solvent mixture and kept at –78 °C for 72 h. Analytically pure colorless crystals were isolated at –78 °C (93%). (Anal. Calcd. for  $\text{C}_{42}\text{H}_{95}\text{Si}_3\text{O}_{14}\text{Ta}$  (%): C, 46.31; H, 8.97. Found: C, 46.37; H, 8.59. FTIR ( $\text{cm}^{-1}$ ): 1389 w, 1365 m, 1242 m, 1192 m, 1114 m, 1071 s, 944 s, 831 w, 802 vw, 701 m, 651 vw, 568 w, 550 w sh, 514 vw, 490 w sh, 469 m, 457 w sh, 433 w.  $^1\text{H}$  NMR (benzene- $d_6$ , 25 °C, 400 MHz):  $\delta$  5.49 (sept, 2 H,  $J$  = 6.1 Hz,  $\text{Ta}(\text{O}^i\text{Pr})$ ), 1.52 (s, 81 H,  $\text{Si}(\text{O}^t\text{Bu})$ ), 1.46 (d, 12 H,  $J$  = 6.1 Hz,  $\text{Ta}(\text{O}^i\text{Pr})$ ).  $^{13}\text{C}\{^1\text{H}\}$  NMR (benzene- $d_6$ , 25 °C, 100 MHz):  $\delta$  75.28  $\text{Ta}(\text{O}^i\text{Pr})$ , 72.91  $\text{Si}(\text{O}^t\text{Bu})$ , 31.87  $\text{Si}(\text{O}^t\text{Bu})$ , 26.96  $\text{Ta}(\text{O}^i\text{Pr})$ .  $^{29}\text{Si}\{^1\text{H}\}$  NMR (benzene- $d_6$ , 25 °C, 99.4 MHz):  $\delta$  –97.57.)

### 2.3. Gelation of **1** in toluene [ $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$ ]

A toluene solution of **1** (0.361 g, 0.06 M) was sealed in a 20-ml Parr reactor in a drybox under a nitrogen atmosphere. The reactor was placed in a preheated oven (180 °C) for 24 h. The wet gel was removed and air-dried for 1 week to form a xerogel. The xerogel was rinsed with pentane ( $2 \times 5$  ml) and toluene ( $2 \times 5$  ml) and was allowed to air-dry for 1 day. The off-white xerogel was ground into a fine powder and dried in vacuo for 12 h at 120 °C to yield 0.110 g of material. Repeated syntheses of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  yielded materials with similar carbon and hydrogen contents, and the same surface areas (within experimental error).

### 2.4. Gelation of **1** and $(^t\text{BuO})_3\text{SiOH}$ in toluene [ $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ ]

A 6.0-ml toluene solution of **1** (0.462 mol) and  $(^t\text{BuO})_3\text{SiOH}$  (2.760 mol) was sealed in a 20-ml Parr reactor in a drybox under a nitrogen atmosphere. The reactor was placed in a preheated oven (180 °C) for 24 h. The wet gel was removed and air-dried for 7 days to form a xerogel. The xerogel was rinsed with hexanes ( $2 \times 5$  ml) and toluene ( $2 \times 5$  ml) and was allowed to air-dry for 1 day. The off-white xerogel was ground into a fine powder and dried in vacuo for 12 h at 120 °C to yield 0.323 g of material.

### 2.5. Preparation of TaSBA-15

The SBA-15 was dried at 130 °C in vacuo for 15 h and handled under a nitrogen atmosphere thereafter. A 0.121-g sample of SBA-15 was suspended in pentane (25 ml). A pentane solution (30 ml) of **1** (0.016 g) was prepared and then added to the stirred suspension of SBA-15 (25 °C). The resulting mixture was stirred for 15 h and then filtered and washed with pentane ( $3 \times 20$  ml). The grafted material was dried for 2–3 h in vacuo to yield the as-prepared catalyst with 1.51 wt% tantalum loading ( $\text{TaSBA-15}$ ,  $\text{SA} = 310 \text{ m}^2 \text{ g}^{-1}$ ), as determined by inductively coupled atomic emission spectroscopy (ICPAES). A subsequent catalyst was prepared by calcination of this material to 300 °C ( $10^\circ\text{C min}^{-1}$ ) under a flow of oxygen for 4 h.

### 2.6. Catalysis procedure

A sample of catalyst (0.035 g) was added to a 50-ml round-bottom flask that was fitted with a reflux condenser and a septum. Acetonitrile (5.0 ml) and cyclohexene (2.5 ml) were added by syringe through the septum under a flow of nitrogen. Dodecane (50.0  $\mu\text{l}$ ) or toluene (23  $\mu\text{l}$ ) was added as an internal standard. The mixture was allowed to equilibrate at the reaction temperature of 65 °C for 10 min. Aqueous  $\text{H}_2\text{O}_2$  (0.62 ml), CHP (1.0 ml), or TBHP (1.0 ml) was added by syringe to the rapidly stirred solution. Aliquots (ca. 0.08 ml) were removed from the reaction mixture by syringe after 5, 30, 60, 90, and 120 min and then filtered and

cooled. The filtrate was analyzed by gas chromatography (GC), and assignments were made by comparison with authentic samples analyzed under the same conditions.

### 2.7. Characterization

Solution  $^1\text{H}$  NMR spectra were recorded at 400 MHz with a Bruker AM-400 spectrometer and were referenced internally to the residual solvent proton signal relative to tetramethylsilane. Similarly, solution  $^{13}\text{C}$  and  $^{29}\text{Si}$  NMR spectra were recorded at 100 and 99.4 MHz, respectively.  $^{29}\text{Si}$  MAS NMR data were collected on a CMX400 Infinity spectrometer based on a 9.4-T magnet, with a frequency of 79.4867 MHz, a spectrum width of 50 kHz, a  $90^\circ$  pulse length of 4  $\mu\text{s}$ , and a pulse delay of 30 s. A direct polarization pulse sequence was used with a 3- $\mu\text{s}$  pulse length. Tetramethylsilane was used as an external chemical shift reference, and samples were spun at 7–10 kHz. Infrared spectra were recorded as KBr disks with a Mattson FTIR spectrometer. Elemental analyses were performed at the College of Chemistry microanalytical laboratory at the University of California, Berkeley, and Galbraith Laboratories, Inc. PXRD experiments were performed on a Siemens D5000 X-ray diffractometer with the use of  $\text{Cu-K}\alpha$  radiation. Transmission electron microscopy was carried out on a Topcon EM-002B transmission electron microscope operating at 200 kV. Samples for energy-dispersive spectroscopy (EDS) were studied on a JEOL JEM-200CX transmission electron microscope operating at 160 kV. EDS spectra were taken on a Gatan detector connected to the electron microscope, and atomic compositions were quantified with the use of the Si- $K$  and Ta- $L$  lines. We prepared samples for TEM studies by depositing a pentane suspension of the finely ground xerogels on carbon-coated copper or gold grids obtained from Ted Pella, Inc. Nitrogen adsorption isotherms were performed on a Quantachrome Autosorb 1 surface area analyzer, and samples were outgassed at  $120^\circ\text{C}$  for at least 15 h prior to measurement. Thermal analyses were performed on a TA Instruments SDT 2960 Integrated TGA/DSC analyzer at a heating rate of  $10^\circ\text{C min}^{-1}$  under a flow of nitrogen or oxygen. Calcinations were performed with the use of a Lindberg  $1200^\circ\text{C}$  three-zone furnace at a heating rate of  $10^\circ\text{C min}^{-1}$  under a flow of oxygen, and the temperature was held constant for 4 h. GC analyses were performed with an HP 6890 GC system and a methyl siloxane capillary ( $50.0\text{ m} \times 320\text{ }\mu\text{m} \times 1.05\text{ }\mu\text{m}$  nominal), and integration was performed relative to dodecane or toluene.

### 2.8. Structural determination for **2**

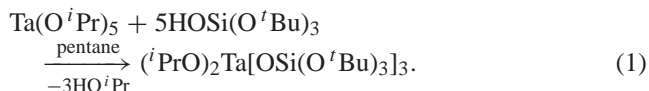
Crystals of **2** were grown from a concentrated pentane solution at  $-40^\circ\text{C}$ . A colorless blocky crystal with dimensions of  $0.36 \times 0.30 \times 0.25\text{ mm}$  was mounted on a glass fiber with Paratone N hydrocarbon oil. Data were collected with a Siemens SMART diffractometer with a CCD area detector. We determined a preliminary orientation matrix and

unit cell parameters by collecting 60 10-s frames, followed by spot integration and least-squares refinement. A hemisphere of data was collected with  $\omega$  scans of  $0.3^\circ$  and a collection time of 10 s per frame. Frame data were integrated ( $XY$  spot spread =  $1.60^\circ$ ;  $Z$  spot spread =  $0.60^\circ$ ) with the use of SAINT. The data were corrected for Lorentz and polarization effects. An absorption correction was performed with XPREP ( $\mu R = 0.2$ ,  $T_{\text{max}} = 0.62$ ,  $T_{\text{min}} = 0.50$ ). The 22,872 integrated reflections were averaged in point group  $2/m$  to give 8238 unique reflections ( $R_{\text{int}} = 0.050$ ). Of these, 4953 reflections were considered to be observed ( $I > 3.00\sigma(I)$ ). No decay correction was necessary. Inspection of the systematic absences uniquely defined the space group  $P2_1/n$ . The structure was solved with direct methods (SIR92) and refined by full matrix least-squares methods with teXsan software. Four oxygen atoms that were modeled as disordered over two sites [O(9)–O(10), O(11)–O(12), O(15)–O(16), O(17)–O(18)] were refined isotropically. The remaining non-hydrogen atoms were refined anisotropically. The hydrogen atoms were included at calculated positions but not refined. The number of variable parameters was 519, giving a data/parameter ratio of 9.54. The maximum and minimum peaks on the final difference Fourier map corresponded to 1.85 and  $-1.70\text{ e}/\text{\AA}^3$ :  $R = 0.044$ ,  $R_w = 0.064$ , GOF = 2.11.

## 3. Results and discussion

### 3.1. Synthesis and characterization of $(^i\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$ (**1**)

The tantalum complex (**1**) was prepared by the addition of a pentane solution of  $(^i\text{BuO})_3\text{SiOH}$  (5 equiv) to a pentane solution of  $\text{Ta}(\text{O}^i\text{Pr})_5$



The product,  $(^i\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$  (**1**), was crystallized from a pentane/toluene mixture (50/50, vol/vol) at  $-78^\circ\text{C}$  to yield analytically pure, colorless crystals. For comparison, Wolczanki has reported tantalum complexes containing no more than three silox ( $^i\text{Bu}_3\text{SiO}-$ ) ligands [39]. In contrast, Bradley has reported the homoleptic siloxide  $\text{Ta}(\text{OSiMe}_3)_5$  as containing the less sterically demanding  $-\text{OSiMe}_3$  ligand [40].

Crystals of sufficient quality to acquire a single-crystal X-ray structure of **1** could not be obtained, but an analogous precursor,  $(\text{EtO})_2\text{Ta}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$  (**2**), was synthesized in a similar fashion. The structure of **2** was unequivocally determined by single-crystal X-ray structure analysis.<sup>1</sup> The

<sup>1</sup> Crystallographic data for **2**. Crystal dimensions (mm):  $0.36 \times 0.30 \times 0.25$ . Crystal system: monoclinic. Space group:  $P2_1/n$ . Unit cell dimensions and volume:  $a = 13.7006(2)\text{ }\text{\AA}$ ,  $b = 16.9122(1)\text{ }\text{\AA}$ ,  $c = 24.1526(4)\text{ }\text{\AA}$ ,

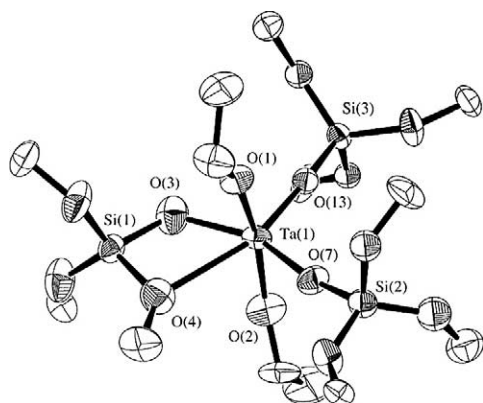


Fig. 1. ORTEP diagram of  $(\text{EtO})_2\text{Ta}[\text{OSi}(\text{O}^t\text{Bu})_3]_3$  (**2**) at the 50% probability level. Terminal methyl groups (on the  $^t\text{BuO}$  groups) and hydrogen atoms have been omitted for clarity.

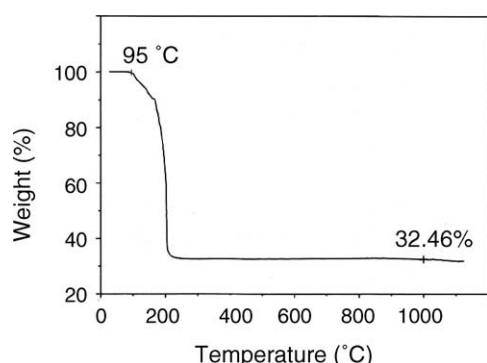


Fig. 2. TGA trace for **1** under a flow of nitrogen, with a heating rate of  $10^\circ\text{C min}^{-1}$ .

ORTEP diagram of **2** is shown in Fig. 1, and bond distances and angles are reported in the [Supplementary Information](#). In complex **2** the five covalently bound ligands, in addition to one datively bound  $\text{O}^t\text{Bu}$  group, form an approximately octahedral coordination environment about the tantalum metal center. This type of bonding mode for a datively bound  $\text{O}^t\text{Bu}$  group from the  $-\text{OSi}(\text{O}^t\text{Bu})_3$  ligand has been observed previously in the solid-state structures of  $\text{Zr}[\text{OSi}(\text{O}^t\text{Bu})_3]_4$  and  $\text{Hf}[\text{OSi}(\text{O}^t\text{Bu})_3]_4$  [41]. The Ta–OSi bond distances ranged from 1.860(5) to 2.041(7) Å and are similar to the Ta–OSi bond distances (1.80–1.94 Å) previously determined for silica-supported tantalum by EXAFS analysis [42].

### 3.2. Thermolytic conversion of **1** to $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$

The decomposition behavior of **1** was studied by thermogravimetric analysis (TGA). The TGA trace for **1** (Fig. 2) shows an onset for weight loss at ca.  $95^\circ\text{C}$  with a precipitous weight loss occurring at ca.  $200^\circ\text{C}$  (under flowing

nitrogen, heated at  $10^\circ\text{C min}^{-1}$ ). After heating to  $1000^\circ\text{C}$ , a ceramic yield of 32.5% was obtained, which is 4.3% lower than the expected ceramic yield for stoichiometric formation of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (36.8% expected). Analysis of the volatile by-products (by  $^1\text{H}$  NMR spectroscopy), trapped from the solid-state decomposition of **1** by vacuum transfer, revealed a significant quantity of  $(^t\text{BuO})_3\text{SiOH}$  (0.32 equiv) in addition to isobutylene. The volatilization of silanol is responsible for the slightly reduced ceramic yields observed by TGA. The solubility of **1** in organic solvents makes it possible to carry out the thermal decomposition in solution. The decomposition of **1** was monitored by solution  $^1\text{H}$  NMR spectroscopy and the quantification of the soluble decomposition products against an internal standard (ferrocene) in benzene- $d_6$ . Heating at  $160^\circ\text{C}$  for 24 h resulted in the complete conversion of **1**; the major products observed were isobutylene (7.5 equiv) and isopropanol (1.3 equiv). Gel formation was observed within 2 h.

Bulk samples of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  were obtained via solution-phase thermolyses ( $150$ – $180^\circ\text{C}$ ) of **1** in isooctane or toluene (ca. 0.06 M) in a sealed Parr reactor under an atmosphere of nitrogen for 24 h. This produced white gels that occupied the entire volume of the original solution. Upon air-drying for several days, the gels shrank to ca. 30% of their original volume and became hard, white materials. The gels were washed with pentane and toluene and then air-dried again overnight. The final xerogels were then ground into a fine powder and dried in vacuo ( $120^\circ\text{C}$ ) for 12 h to provide the as-prepared  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  material.

### 3.3. Co-thermolytic synthesis of $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$

Previously we reported the co-thermolysis of a zirconium-containing molecular precursor with  $\text{Si}(\text{OEt})_4$  (TEOS) to produce homogeneous zirconia–silica materials with tunable silicon to zirconium ratios [27]. Similarly, co-thermolyses of the tantalum-containing molecular precursor (**1**) with  $(^t\text{BuO})_3\text{SiOH}$  readily yielded tantalum–silica materials. Notably, the silanol ligand does not thermally convert to silica in the absence of tantalum. Solution  $^1\text{H}$  NMR spectroscopic studies demonstrated that heating benzene- $d_6$  solutions of **1** and  $(^t\text{BuO})_3\text{SiOH}$  (1:5.2 mol ratios) to  $160^\circ\text{C}$  resulted in gel formation within 2 h. The precursors  $(^t\text{BuO})_3\text{SiOH}$  and **1** were completely consumed and incorporated into the material after 2 h, and isobutylene (25 equiv) was quantitatively observed as the only decomposition product. Increasing the molar ratio of **1** to  $(^t\text{BuO})_3\text{SiOH}$  beyond 1/6 resulted in incomplete thermal decomposition of  $(^t\text{BuO})_3\text{SiOH}$  after heating at  $160^\circ\text{C}$  for 24 h.

Bulk samples of  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  were prepared by combining **1** and  $(^t\text{BuO})_3\text{SiOH}$  (1/6 mol ratio) in a toluene solution and heating in a Parr reactor under nitrogen at  $180^\circ\text{C}$  for 24 h. This preparation yielded a monolithic, white gel that was air-dried for 1 week, washed with hexanes and toluene, and then air-dried again for 1 day. The final xerogel was then

$\beta = 93.049(1)^\circ$ ,  $V = 5588.1(1) \text{ \AA}^3$ ,  $\rho_{\text{calc}} = 1.261 \text{ g cm}^{-3}$ . Radiation: Mo- $\text{K}\alpha$  ( $\lambda = 0.71069 \text{ \AA}$ ). Scan type:  $\omega$  (0.3 degrees per frame). Temperature of measurement:  $-110^\circ\text{C}$ . No. of reflections measured: total = 22,872, unique = 8238.  $R_{\text{obs}} = 0.044$ ,  $wR2_{\text{obs}} = 0.064$ ,  $\text{GOF}_{\text{obs}} = 2.11$ .



ground into a fine powder and dried in vacuo at 120 °C for 12 h.

### 3.4. Characterization of tantalum–silica materials

By elemental analysis (inductively coupled plasma atomic emission spectroscopy), the Si/Ta ratio for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  was found to be 2.88/1, which is very close to the expected ratio of 3/1. The elemental composition and homogeneity for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  were probed by energy-dispersive X-ray spectroscopy (EDS). EDS profiles taken from local portions (ca. 30 nm) of the  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  xerogel revealed a Si/Ta ratio of 8.34/1, which is within 10% of the expected value and constant over randomly sampled local areas. The carbon content for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  was found to be quite low (0.72%) by combustion analysis. After calcination to 500 °C under flowing oxygen, the carbon content remained unchanged (0.75%). The carbon content for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  was found to be 2.61% by combustion analysis and 0.25% after calcination to 500 °C under flowing oxygen. Carbon in the uncalcined, silica-rich  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  xerogel most likely comes from *tert*-butyl groups from  $\text{HOSi}(\text{O}^t\text{Bu})_3$  added to the thermolysis mixture and is not uncommon for the thermolytic molecular precursor route [27]. Thermogravimetric analysis of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  with a heating rate of 10 °C min<sup>−1</sup> under oxygen revealed a mass loss of 3.4% up to 350 °C, which probably corresponds to physisorbed and chemisorbed water and organic species [43]. Likewise for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ , TGA revealed a mass loss of 4.6% when heated to 350 °C. Heating these materials to 1000 °C resulted in an additional 1.0–3.0 wt% loss.

The crystallization behavior of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  as a function of temperature was studied by powder X-ray diffraction (PXRD). The xerogel derived from **1** remained amorphous up to 1100 °C, when domains of the orthorhombic, low-temperature form of  $\text{Ta}_2\text{O}_5$  (L- $\text{Ta}_2\text{O}_5$ ) were detected [44]. Upon further calcination to 1300 °C the peaks in the PXRD spectrum sharpened with increasing crystallite size. The xerogel derived from the co-thermolysis of **1** and  $\text{HOSi}(\text{O}^t\text{Bu})_3$  remained amorphous until the temperature went above 1000 °C, where domains of L- $\text{Ta}_2\text{O}_5$  were first detected by very broad features in the PXRD pattern. As with other multicomponent mixed-oxide ceramics, the temperature at which a single-component phase segregates and crystallizes can be used as a gauge of the original homogeneity of the mixed-oxide material. For homogeneous mixed oxides, more extensive diffusion must occur prior to nucleation and grain growth of the crystalline phase [43,45,46]. This will delay the appearance of crystalline single-component oxides. Bulk  $\text{Ta}_2\text{O}_5$  crystallizes into L- $\text{Ta}_2\text{O}_5$  at ca. 750 °C, whereas  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  required calcination to a temperature above 1000 °C before L- $\text{Ta}_2\text{O}_5$  was observed. Similarly, Guio and Grange found that a sol–gel-derived  $\text{Ta}_2\text{O}_5 \cdot 5.2\text{SiO}_2$  mixed oxide required calcination to 1200 °C before crystalline L- $\text{Ta}_2\text{O}_5$  was observed [43].

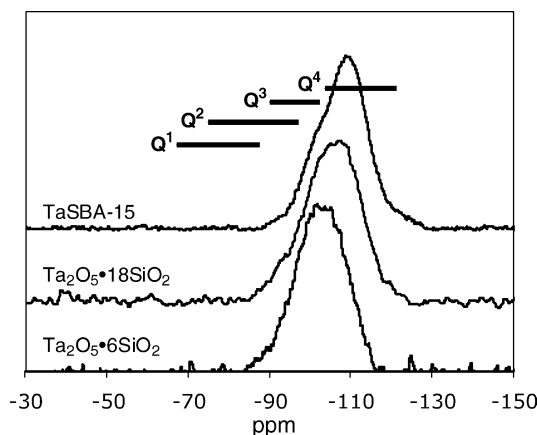


Fig. 3.  $^{29}\text{Si}$  MAS NMR spectra of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$ ,  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ , and TaSBA-15 showing  $\text{Q}^1$ ,  $\text{Q}^2$ ,  $\text{Q}^3$ , and  $\text{Q}^4$  ranges of chemical shifts from inorganic framework silicon atoms.

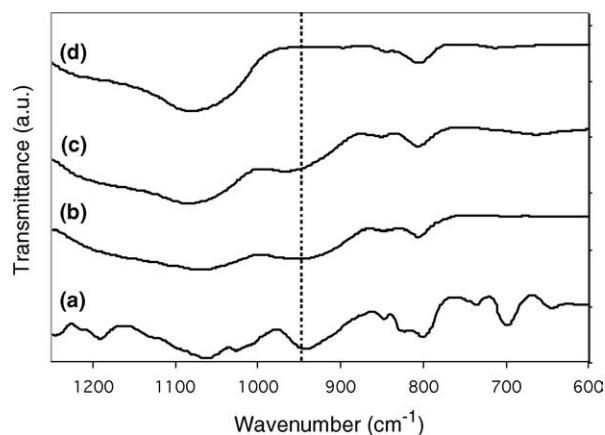


Fig. 4. Room temperature FTIR spectra of **1** (a),  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (b),  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (c), and TaSBA-15 (d). The Ta–O–Si asymmetric stretching band is highlighted with a dashed line.

The molecular precursor **1** can serve as a spectroscopic model for tantalum–silica materials. The observed  $^{29}\text{Si}$  NMR resonance for **1** at  $-97.57$  ppm is in the region expected for  $\text{M–OSi}(\text{O}^t\text{Bu})_3$  sites. The silicon environments of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  were examined by solid-state  $^{29}\text{Si}$  MAS NMR spectroscopy with the use of direct polarization and are typical of amorphous silica networks (Fig. 3). The  $^{29}\text{Si}$  MAS NMR spectra reveal broad resonances centered at  $-103$  ppm for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $-108$  ppm for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  that span the chemical shift range for  $\text{Q}^2$ ,  $\text{Q}^3$ , and  $\text{Q}^4$  silicon environments. The  $^{29}\text{Si}$  NMR spectrum for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  is shifted toward the  $\text{Q}^4$  ( $\text{Si–}(\text{OSi})_4$ ) chemical shift range, as expected for the more silicon-rich xerogel. The FTIR spectrum of **1** exhibits strong Si–O–Si and Si–O–C overlapping bands centered at  $1065$  cm<sup>−1</sup> (Fig. 4). A strong band centered at  $944$  cm<sup>−1</sup> is observed for the Ta–O–Si asymmetric stretching mode [47,48]. The FTIR spectra of both  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  display a strong band for Si–O–Si at  $1085$  and  $1078$  cm<sup>−1</sup>, respectively. Both materials exhibit the characteristic band at  $951$  and  $969$  cm<sup>−1</sup>, respectively, for the Ta–O–Si asym-

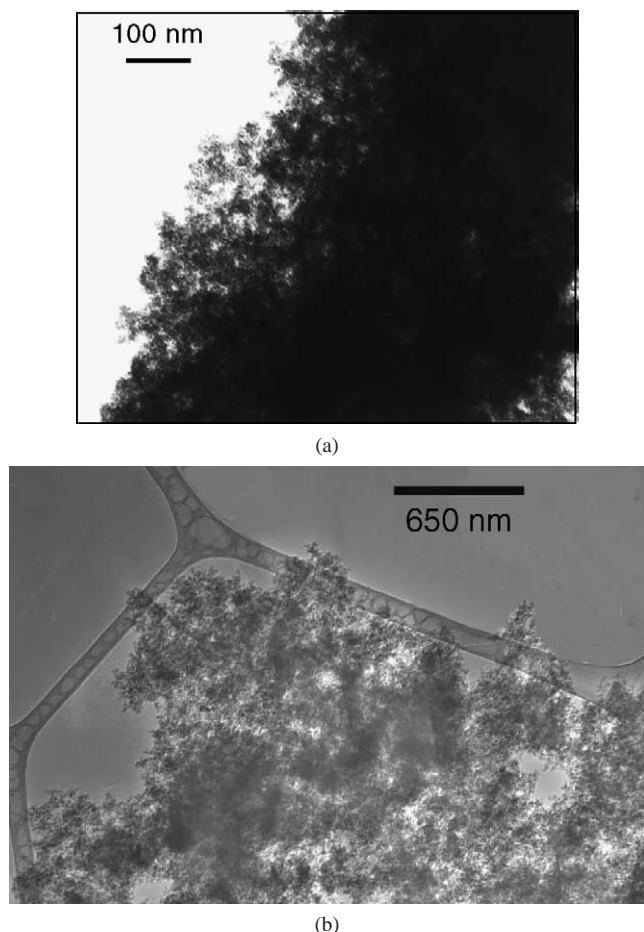


Fig. 5. TEM micrographs of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (a) and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (b).

metric stretching mode [43,49,50]. These observed bands at ca.  $960\text{ cm}^{-1}$  are generally thought of as an overlap of two contributions (i.e., from the Ta–O–Si asymmetric stretching mode and the Si–OH mode). After calcination of these materials to  $500^\circ\text{C}$  under flowing oxygen, the band for Ta–O–Si is still observed, suggesting that a high number of Ta–O–Si linkages remain intact.

Transmission electron microscopy (TEM) studies of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  revealed aggregates of fine granules with a wide range of particle sizes, as shown in Fig. 5. Nitrogen porosimetry was used to further evaluate the pore structures and surface areas of the tantalum-silica materials (Fig. 6). The adsorption–desorption data for both  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  correspond to type IV isotherms [51], suggesting some mesoporosity; however, a steep rise in adsorbed volume at relative pressure ( $P/P_0$ )  $> 0.8$  is indicative of textural porosity [52]. The isotherm for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  displays an H1 hysteresis (IUPAC classification) that is indicative of a porous material consisting of voids between agglomerates (i.e., rigidly joined particles) [51]. The isotherm for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ , on the other hand, displays an H3 hysteresis that is indicative of an almost nonporous material consisting of aggregates (i.e., loosely coherent particles) [51]. In both cases, the materi-

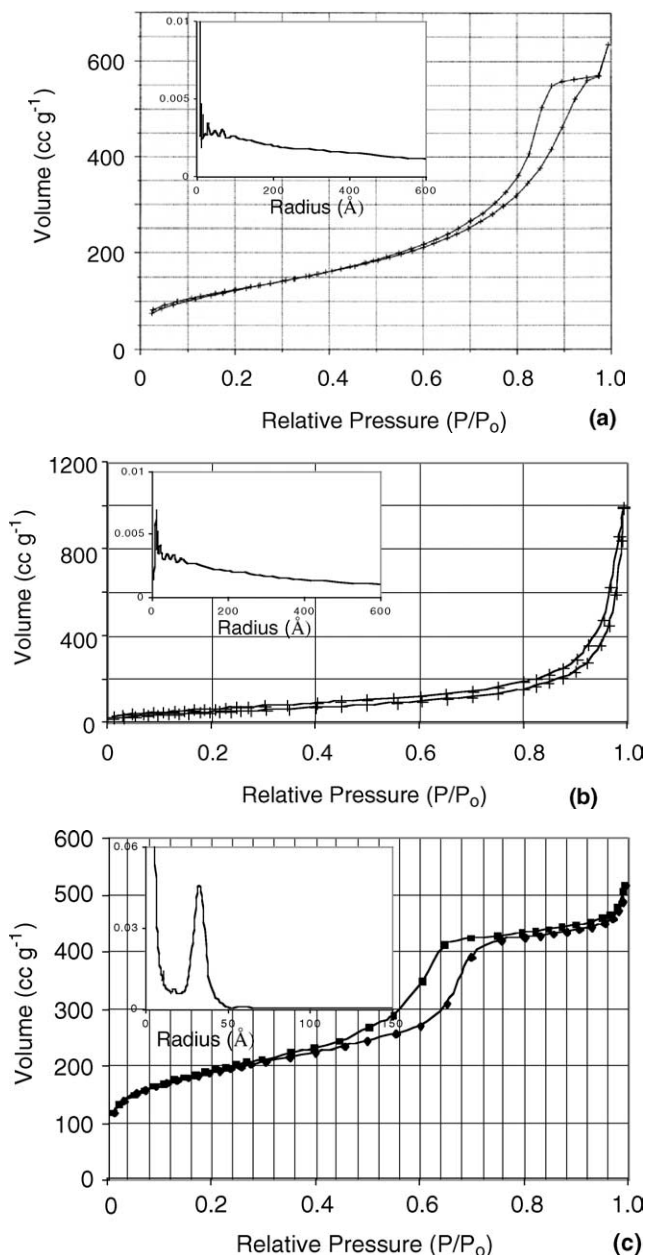


Fig. 6. Nitrogen adsorption–desorption isotherms for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (a) and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (b), and TaSBA-15 (c). Pore size distributions calculated from the adsorption isotherm branch are shown as insets.

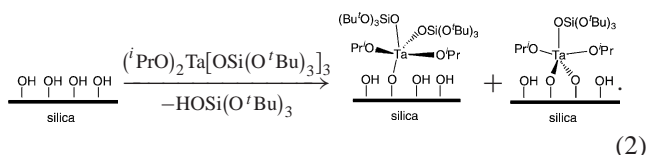
als possess a wide range of pore sizes, with a considerable amount of micropores with radii smaller than  $20\text{ Å}$  (Fig. 6). The materials were found to have relatively high BET surface areas [53], ranging from  $450\text{ m}^2\text{ g}^{-1}$  for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  to  $200\text{ m}^2\text{ g}^{-1}$  for  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ . It has similarly been observed that co-thermolysis of the  $\text{Zr}[\text{OSi}(\text{O}'\text{Bu})_3]_4$  molecular precursor with TEOS resulted in a surface area lower than that of the parent  $\text{ZrO}_2 \cdot 4\text{SiO}_2$  material [27]. Calcination of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  to  $500^\circ\text{C}$  under oxygen did not result in a change in surface area ( $440\text{ m}^2\text{ g}^{-1}$ ), and likewise calcination of  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  to  $500^\circ\text{C}$  resulted in essentially no change in surface area ( $220\text{ m}^2\text{ g}^{-1}$ ). Calcination of these

materials to 1000 °C resulted in a substantial loss of surface area (to  $< 5 \text{ m}^2 \text{ g}^{-1}$ ), however.

### 3.5. Synthesis and characterization of surface-supported TaSBA-15

In addition to the tantalum–silica xerogels, a catalyst was prepared by grafting **1** onto a mesoporous SBA-15 substrate ( $\text{SA} = 690 \text{ m}^2 \text{ g}^{-1}$ , OH coverage =  $2.0 \text{ nm}^{-2}$ ). The grafting was accomplished via the addition of **1** (0.015 mmol) to the substrate (120 mg) to give a material with 1.51 wt% ( $\text{Si/Ta} = 200/1$ ) tantalum loading, as determined by inductively coupled atomic emission spectroscopy (ICPAES). A subsequent catalyst was prepared by calcination of the TaSBA-15 material to 300 °C under oxygen to remove the organic moieties of the molecular precursor. This low weight loading should result in single-site tantalum centers on the silica surface [25,26]. Furthermore, the grafted materials have surface areas ( $310 \text{ m}^2 \text{ g}^{-1}$ ) that are reduced relative to that of the SBA-15 support; however, their ordered mesostructure was maintained, as evidenced by retention of the low-angle (100) reflection in the powder X-ray diffraction pattern. The adsorption–desorption data for TaSBA-15 correspond to a type IV isotherm, characteristic of mesoporous SBA-15 materials (Fig. 6c) [25]. The pore size distribution was observed to be relatively narrow, and the average pore radius, as determined by the nitrogen adsorption isotherm, was 33 Å. The pore structure of TaSBA-15 stands in contrast with that of the  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  xerogels, in that it has a well-defined, mesoporous, hexagonally ordered pore structure (by nitrogen porosimetry and low-angle X-ray diffraction).

Solution  $^1\text{H}$  NMR spectroscopy was used to monitor the grafting chemistry of **1**. The reaction of surface Si–OH groups with **1** resulted in the elimination of 1.5 equiv of  $(^i\text{BuO})_3\text{SiOH}$  per grafted molecule of **1**. This suggests that the tantalum species bind to the silica surface via 1 or 2 Si–O–Ta linkages, and that the two structures are equally abundant



Also, based on the initial OH coverage of the support, the precursor reacts with only ca. 6% of the available OH sites with a 1.51 wt% Ta loading. The exact structure of the surface-bound Ta species is currently unknown, however, because of a lack of spectroscopic handles for such a low-abundance species. The observed band at ca.  $960 \text{ cm}^{-1}$  for the Ta–O–Si asymmetric stretching mode is not observed in the FTIR spectrum (Fig. 4), presumably as a result of the low Ta wt%. The M–O–Si stretching mode was also not observed in similarly prepared TiSBA-15 materials [25]. Furthermore, the  $^{29}\text{Si}$  MAS NMR spectrum for TaSBA-15 reveals a broad resonance centered at  $-110 \text{ ppm}$  that spans the chemical shift range for  $\text{Q}^2$ ,  $\text{Q}^3$ , and  $\text{Q}^4$  silicon environments (Fig. 3). The resonance for TaSBA-15 is further shifted toward the  $\text{Q}^4$  chemical shift range as compared with the spectra for  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$ , suggesting a more fully condensed  $\text{SiO}_2$  network.

### 3.6. Catalytic oxidation of cyclohexene

Samples of  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (calcined to 500 °C) were found to exhibit catalytic activity for the oxidation of cyclohexene with TBHP, CHP, and aqueous  $\text{H}_2\text{O}_2$  as the oxidants. The surface-supported TaSBA-15 catalyst was also found to be active for the oxidation of cyclohexene with TBHP, CHP, and aqueous  $\text{H}_2\text{O}_2$ .

To compare the activities for the heterogeneous catalysts (Table 1), we standardized the results with respect to mass of catalyst (0.035 g). In control experiments with catalyst and no oxidant, or with oxidant and no catalyst, no cyclohexene oxidation products were observed by GC analysis. In addition, catalysts were stirred in acetonitrile and cyclohexene for 1 h at 65 °C before addition of the oxidant. The solution was then hot-filtered after 10 min and stirred for 2 h at 65 °C. There was no significant oxidation of cyclohexene after the hot filtration, suggesting that leaching of catalytically active, soluble tantalum species is negligible under these experimental conditions.

In Fig. 7, the results of cyclohexene oxidation with the use of several tantalum–silica catalysts (on a per-gram basis) are depicted. The TaSBA-15 catalyst exhibited a higher activity for the oxidation of cyclohexene than the tantalum–silica xerogels after 2 h. Use of TaSBA-15 as the catalyst (65 °C in acetonitrile) with  $\text{H}_2\text{O}_2$  yielded 13.6% of oxidation products after 2 h (based on oxidant), whereas  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and

Table 1  
Tantalum-catalyzed oxidation of cyclohexene with  $\text{H}_2\text{O}_2$  (65 °C, reaction time = 2 h)

Catalyst	Selectivity cyclohexene oxide (%)	Selectivity cyclohexenol (%)	Selectivity cyclohexenone (%)	Total yield based on $\text{H}_2\text{O}_2$ (%)	Initial rate <sup>a</sup> (mol oxidation products/(molTa(V) cat min))
$\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$	9.60	58.6	31.8	2.61	0.13
$\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$	17.2	37.9	44.9	4.70	0.22
TaSBA-15	36.0	32.7	31.3	13.6	6.70
TaSBA-15 (300 °C)	42.7	25.3	32.0	5.32	3.45

<sup>a</sup> Initial rate measured as the slope of the tangent to the plot of concentration versus time at  $t = 0$ , normalized per mol of Ta(V).



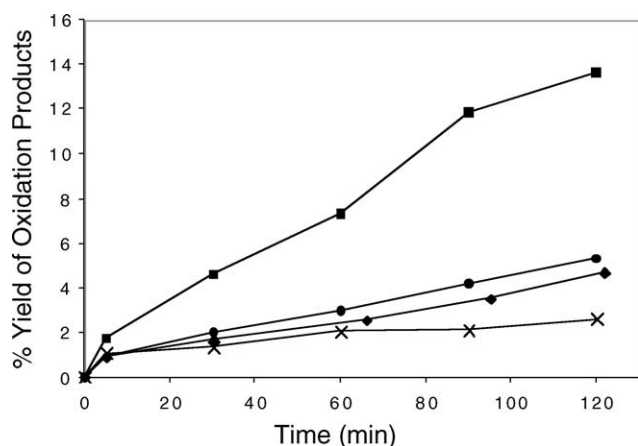


Fig. 7. Yield of cyclohexene oxidation products relative to initial  $\text{H}_2\text{O}_2$  concentration as a function of time during the oxidation of cyclohexene with 0.035 g of TaSBA-15 (■), TaSBA-15 (300 °C) (●),  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (◆), and  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (×).

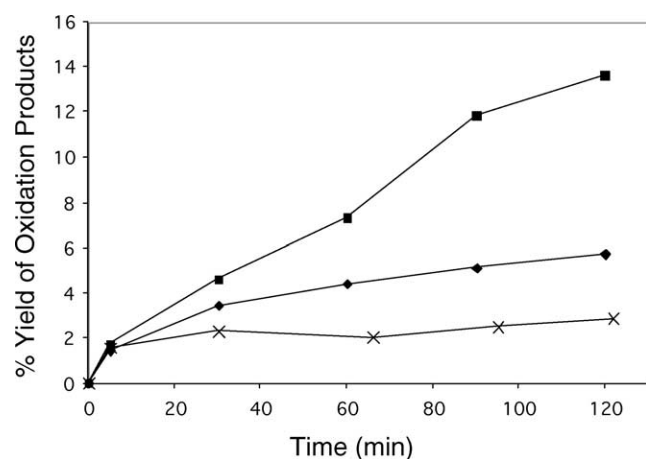


Fig. 8. Yield of cyclohexene oxidation products relative to initial  $\text{H}_2\text{O}_2$  (■), CHP (◆), and TBHP (×) concentrations as a function of time during the oxidation of cyclohexene with 0.035 g of TaSBA-15.

$\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  under analogous conditions yielded 2.6% and 4.7% of oxidation products, respectively. Calcination of the TaSBA-15 material to 300 °C under oxygen yielded a catalyst with lower activity (5.3% yield of cyclohexene oxidation as compared with 13.6%), which is consistent with previous results on titanium-based catalysts [25]. Calcination may result in migration of the tantalum into the framework silica, possibly facilitated by the siloxide ligands of **1** that would be converted to new surface silica centers. The TaSBA-15 catalysts are more selective for cyclohexene oxide formation (36–43%, 2 h), and  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  and  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  are less selective (10 and 17%, respectively). Over the course of 2 h, the selectivity for cyclohexene oxide drops as the abundance of allylic oxidation products increases (e.g., initial selectivity of 52% for cyclohexene oxide with the TaSBA-15 catalyst).

The results of cyclohexene oxidation with TaSBA-15 and three different oxidants (TBHP, CHP, and  $\text{H}_2\text{O}_2$ ) are shown in Fig. 8. It appears that aqueous  $\text{H}_2\text{O}_2$  is the most active

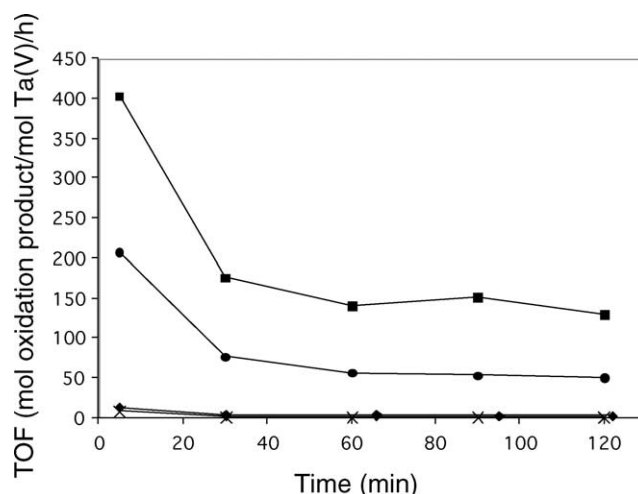


Fig. 9. Turnover frequencies (TOFs) as a function of time during the oxidation of cyclohexene with TaSBA-15 (■), TaSBA-15 (300 °C) (●),  $\text{Ta}_2\text{O}_5 \cdot 18\text{SiO}_2$  (◆), and  $\text{Ta}_2\text{O}_5 \cdot 6\text{SiO}_2$  (×). TOF = moles of cyclohexene oxidation products per mol Ta(V) per hour.

oxidant; the two organic peroxides have comparably lower activities. The selectivities achieved with the different oxidants are markedly different, however. Use of the organic peroxides results in high selectivities for cyclohexene oxide formation (94 and 70% with CHP and TBHP, respectively), whereas  $\text{H}_2\text{O}_2$  is much less selective for epoxidation (36%).

Fig. 9 illustrates the catalyst activities in turnover frequencies (TOF), defined as the moles of oxidation product per mole Ta(V) per hour. The cyclohexene oxidation is generally more rapid (regardless of oxidant or catalyst) over the first 30 min of the reaction, and then the reaction slows for the remaining 90 min. This is attributed to increasing quantities of water or alcohol formation with time, thereby hindering formation of the tantalum-hydroperoxide complex by strong binding of polar species [54]. The initial rate of cyclohexene oxidation, as shown in Table 1, was greater with the TaSBA-15 catalysts (initial rate = 6.70 mol oxidation products/(mol Ta(V) cat min)). These results are possibly due to the presence of substrate-available, authentic surface tantalum sites in the mesopores of the TaSBA-15 catalyst. The xerogel catalysts, on the other hand, have considerable amounts of tantalum that are unavailable to substrate throughout the microporous bulk of the material and buried within in the silicate walls. It is well established that cyclohexene cannot be oxidized in a microporous TS1 material because of size constraints for the cyclohexene oxide product [55]. The pores of the TaSBA-15 catalyst should be large enough that diffusion does not limit the reaction rate with acetonitrile as the solvent. The xerogel catalysts, however, have a considerably microporous character and might be affected by diffusion limitations and steric constraints. Potential differences in observed rates caused by diffusion effects, particle size differences, hydrophobicity differences, etc. were not examined. Specific surface areas of the catalysts do not seem to affect the activity of these cat-



alysts, at least in the high-surface-area regime studied here ( $> 200 \text{ m}^2 \text{ g}^{-1}$ ).

The catalyst activities reported here for the oxidation of cyclohexene are comparable to the activities recently reported for niobia–silica catalysts under similar conditions [55]. Hartmann and co-workers reported cyclohexene oxide yields of up to 15% (after 2 h) for microporous crystalline NbS-1 and Nb/silicalite-1 catalysts, with selectivities up to 80% for cyclohexene oxide formation. A mesoporous, noncrystalline NbMCM-41 catalyst provided good yields of cyclohexene oxidation products (ca. 20–45% after 2 h) as well [33,56]. In contrast, previously reported SBA-15-supported, single-site Ti(IV) catalysts are much more active (98% yield of oxidation products) for the oxidation of cyclohexene and give cyclohexene oxide selectively (90–100%) [25]. This Ti(IV) system was limited to the use of organic peroxides (CHP, TBHP), however, with yields less than 5% obtained when aqueous  $\text{H}_2\text{O}_2$  was used. It appears that titanium cyclohexene oxidation catalysts are inherently more active, but comparable group V niobium and tantalum catalysts can operate when aqueous  $\text{H}_2\text{O}_2$  is used as the oxidant.

#### 4. Conclusions

Here we described the preparation and characterization of a new bis(alkoxy)tris(siloxy)tantalum(V) single-source molecular precursor,  $(t\text{PrO})_2\text{Ta}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$  (**1**). This compound represents an interesting model for tantalum sites in silica, and the single-crystal X-ray structure of an analogous compound,  $(\text{EtO})_2\text{Ta}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$  (**2**), provides structural information on such sites. The Ta–OSi bond distances of 1.860(5)–2.041(7) Å are similar to those previously reported by Roesky and co-workers for a model tantalum siloxide cage complex (1.984–1.987 Å) [47]. Both of these model complexes are in good agreement with Ta–OSi bond distances determined for silica-supported tantalum oxide by EXAFS analyses [42,50]. Furthermore, the  $^{29}\text{Si}$  NMR chemical shift for **1** at  $-97.57$  ppm provides an important spectroscopic reference for Ta(V)/ $\text{SiO}_2$  systems. Because of a lack of analogous  $\text{TaOSiO}_3$  model complexes, no direct spectroscopic  $^{29}\text{Si}$  NMR comparisons can be made; however, a series of early transition-metal siloxy complexes of the type  $\text{MOSiO}_3$  ( $\text{M} = \text{Ti}, \text{Zr}, \text{Hf}, \text{V}$ ) has been prepared [41,57,58]. The group IV complexes of the type  $\text{M}[\text{OSi}(\text{O}^i\text{Bu})_3]_4$  exhibit  $^{29}\text{Si}$  NMR resonances at  $-103.24$ ,  $-100.50$ , and  $-97.06$  ppm for  $\text{M} = \text{Ti}, \text{Zr}$ , and  $\text{Hf}$ , respectively. Moreover, a  $\text{V}(\text{V})=\text{O}$  complex of the type  $\text{OV}[\text{OSi}(\text{O}^i\text{Bu})_3]_3$  exhibited a  $^{29}\text{Si}$  NMR resonance at  $-98.00$  ppm. The observed chemical shift for **1** comes where expected, compared with these slightly different early transition-metal siloxy complexes.

In this study it was shown that **1** is a versatile reagent for both the preparation of bulk tantalum–silica xerogels and the grafting of tantalum centers onto the surface of silica. In addition, more silica-rich materials can be obtained through

a co-thermolytic route with **1** and  $\text{HOSi}(\text{O}^i\text{Bu})_3$ . This expands the tunability of the thermolytic molecular precursor route by allowing variable metal-to-silicon ratios. Furthermore, because  $\text{HOSi}(\text{O}^i\text{Bu})_3$  cleanly converts to  $\text{SiO}_2$  via the stoichiometric elimination of isobutylene and water in the presence of tantalum, the presence of incompletely condensed alkoxy groups is avoided, unlike the case with TEOS [27].

To our knowledge, this work represents the first utilization of tantalum–silica materials as cyclohexene oxidation catalysts. The most active catalyst for the oxidation of cyclohexene has grafted tantalum sites (TaSBA-15) and uses  $\text{H}_2\text{O}_2$  as the oxidant in acetonitrile at  $65^\circ\text{C}$  (initial rate of 6.70 mole oxidation product per mole Ta(V) per minute). The organic peroxides TBHP and CHP are also viable and more selective, but less active, oxidants. Conversely, previously reported TiSBA-15 catalysts were extremely active in cyclohexene epoxidation with CHP and TBHP as oxidants but essentially inactive in combination with  $\text{H}_2\text{O}_2$ . This suggests that Ta(V) is more tolerant of the presence of water for cyclohexene oxidant than the analogous Ti(IV) system, which perhaps is a result of an extra coordination site for group V metals, assuming an equal number of surface Si–O–M linkages. It is interesting to note that Basset and co-workers have developed Ta(V)/ $\text{SiO}_2$  catalysts that are very active in the epoxidation of allylic alcohols [29,30]. Given the observed activity of catalysts described here, this suggests that the activity of alkene oxidation by heterogeneous tantalum–silica catalysts is highly substrate dependent.

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#### Supplementary material

Experimental and characterization data and selected bond angles and distances for **2**.

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